## Problem 1 (Individual) - KEY

Consider a two phase $1000 \mathrm{lb}-\mathrm{mole} / \mathrm{hr}$ stream with the following composition: Butane $33 \mathrm{~mol} \%$, Pentane $51 \mathrm{~mol} \%$, Hexane $16 \mathrm{~mol} \%$, at 15 pisa and $130{ }^{\circ} \mathrm{F}$. This is the same mixture used in the previous assignment. It is desired to separate this mixture into two streams. One with $99 \%$ butane and another one with NO MORE THAN $1 \%$ butane.

Use the Fenske method to determine the number of trays that you will approximately need.


Mass Balance:
$F=D+B$
$z_{\text {butane }} F=\left(x_{D}\right) D+\left(x_{B}\right) B$
We assume that $\mathrm{F}=1000 \mathrm{lbmol} / \mathrm{hr}, z_{\text {butane }}=0.33, \mathrm{x}_{\mathrm{D}}=0.99$, and $\mathrm{x}_{\mathrm{B}}=0.01$.
$1000 \frac{\mathrm{lbmol}}{\mathrm{hr}}=D+B$
$0.33\left(1000 \frac{\mathrm{lbmol}}{\mathrm{hr}}\right)=(0.99) D+(0.01) B$

Solving the two equations yields:
$D=326.531 \frac{\mathrm{lbmol}}{\mathrm{hr}}$
$B=673.470 \frac{\mathrm{lbmol}}{\mathrm{hr}}$

Use the Fenske Equation.
$N_{\text {min }}=\frac{\operatorname{LOG}\left[\left(\frac{x_{d}}{1-x_{d}}\right) *\left(\frac{1-x_{b}}{x_{b}}\right)\right]}{\operatorname{LOG}\left(\alpha_{\text {avg }}\right)}$
$\propto_{\frac{\text { butane }}{\text { pentane }}}=\frac{K_{\text {butane }}}{K_{\text {pentane }}}$
$K_{i}=\frac{P_{i}^{s a t}}{P}$
$K_{i}=\frac{10^{A_{i}-\left(\frac{B_{i}}{C_{i}+T}\right)}}{P}$

| F (lbmol/hr) | 1000 |
| :--- | ---: |
| $\mathbf{P}$ (psia) | 35 |
| $\mathbf{P}$ (bar) | 2.41317 |
| T ( ${ }^{\circ} \mathrm{F}$ ) | 130 |
| T (K) | 327.594 |
| $\mathbf{Z}_{\text {butane }}$ | 0.33 |
| $\mathrm{Z}_{\text {pentane }}$ | 0.51 |
| $\mathrm{Z}_{\text {hexane }}$ | 0.16 |


| Butane |  |
| :--- | ---: |
| A | 4.35576 |
| B | 1176.58 |
| $\mathbf{C}$ | -2.071 |
| $\mathbf{P}^{\text {sot }}$ (bar) | 5.51223 |
| $\mathbf{K}$ | 2.28423 |
| $\mathbf{X}$ | 0.22918 |
| $\mathbf{y}$ | 0.52351 |$\quad$| Pentane |  |
| :--- | ---: |
|  | $\mathbf{B}$ |
| $\mathbf{C}$ | 1070.62 |


| Hexane |  |
| :--- | ---: |
| $\mathbf{A}$ | 4.00266 |
| $\mathbf{B}$ | 1171.53 |
| $\mathbf{C}$ | -48.784 |
| $\mathbf{P}^{\text {sot }}$ (bar) | 0.63207 |
| $\mathbf{K}$ | 0.26193 |
| $\mathbf{x}$ | 0.21414 |
| $\mathbf{y}$ | 0.05609 |

$\propto_{\frac{\text { butane }}{\text { pentane }}}=\frac{2.28423}{0.75519}=3.02469$
$N_{\text {min }}=\frac{\operatorname{LOG}\left[\left(\frac{0.99}{1-0.99}\right) *\left(\frac{1-0.01}{0.01}\right)\right]}{\operatorname{LOG(3.02)}}$
$N_{\text {min }}=8.315$
$\sim 8$ trays are needed.

